

## Heat transfer in a simulated spent fuel pool for different types of spent fuels

### Transferência de calor em um pool simulado de combustível queimado para diferentes tipos de combustíveis queimados

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**ABSTRACT**

Historically, the Spent Fuel Pool (SFP) of Angra II, from Brazil, has received standard spent fuel (SF) assemblies of uranium dioxide ( $\text{UO}_2$ ) discharged from Pressurized Water Reactors (PWR) of the Nuclear Power Plants (NPP) of Angra. However, in case of using Mixed Oxide (MOX) or thorium-based fuels at a proportion of 1/3 or 1/4 of the total of fuel assemblies in their PWRs as it has been occurring worldwide, it would require further thermal studies of wet storage of the new mixed SF generated. It includes the determination of the water boiling time ( $T_b$ ) of the SFP in case of breakdown of its external cooling system (ECS). This work presents studies of  $T_b$  of a simulated SFP storing mixed SF discharged from PWRs. The types of mixed SF studied include MOX plus  $\text{UO}_2$ , oxide of thorium/uranium (U-Th) $\text{O}_2$  plus  $\text{UO}_2$ , and oxide of thorium/transuranic (TRU-Th) $\text{O}_2$  plus  $\text{UO}_2$ . All the mixed SF was considered to contain 1/3 or 1/4 of either thorium-based fuels or reprocessed fuel. The simulations were implemented in CFX Ansys and OpenFOAM© codes.  $T_b$  from simulations with Ansys ranged from 4.05 h to 5.97 h, and from 3.45 h to 5.77 h from simulations with OpenFOAM©. Results show that, independent of the mixed loading pattern of the SFP, the water would reach the saturation temperature more rapidly when (TRU-Th) $\text{O}_2$  was present. By contrast, when MOX was present,  $T_b$  was greater.

**Keywords:** Spent fuel pool, OpenFOAM©, CFX Ansys.

**RESUMO**

Historicamente, o Pool de Combustível Irrradiado (SFP) de Angra II, do Brasil, tem recebido montagens de combustível padrão gasto (SF) de dióxido de urânio ( $\text{UO}_2$ ) descarregado de Reatores de Água Pressurizada (PWR) das Usinas Nucleares (NPP) de Angra. Entretanto, no caso de utilização de combustíveis à base de óxido misto (MOX) ou tório na proporção de 1/3 ou 1/4 do total de conjuntos de combustível em suas PWRs como vem ocorrendo em todo o mundo, seriam necessários mais estudos térmicos de armazenamento úmido do novo SF misto gerado. Inclui a determinação do tempo de ebulição da água ( $T_b$ ) do SFP em caso de quebra de seu sistema de resfriamento externo (ECS). Este trabalho apresenta estudos de  $T_b$  de um SFP simulado de armazenamento de SF misto descarregado de PWRs. Os tipos de SF mistos estudados incluem MOX mais  $\text{UO}_2$ , óxido de tório/urânio (U-Th) $\text{O}_2$  mais  $\text{UO}_2$ , e óxido de tório/transurânico (TRU-Th) $\text{O}_2$  mais  $\text{UO}_2$ . Todo o SF misto foi considerado como contendo 1/3 ou 1/4 de combustíveis à base de tório ou combustível reprocessado. As simulações foram implementadas nos códigos CFX Ansys e OpenFOAM©.  $T_b$  de simulações com Ansys variou de 4,05 h a 5,97 h, e de 3,45 h a 5,77 h de simulações com OpenFOAM©. Os resultados mostram que, independente do padrão de carga mista do SFP, a água alcançaria a temperatura de saturação mais rapidamente quando (TRU-Th) $\text{O}_2$  estivesse presente. Em contraste, quando MOX estava presente, a  $T_b$  era maior.

**Palavras-chave:** Pool de combustível gasto, OpenFOAM©, CFX Ansys.

## 1 INTRODUCTION

Aiming at decreasing the utilization of uranium, some nuclear utilities are planning, or have already implemented plutonium recycling schemes in thermal reactors, specially, PWRs. Normally, plutonium is recycled as MOX fuel, in which it is mixed with  $UO_2$  in the form of plutonium dioxide ( $PuO_2$ ) in a same reactor at a proportion of 1/3 or 1/4 [1]. Since 80's, France has been reprocessing SF and recycling the fuel obtained from Pu spiked with depleted uranium (MOX), and inserting it into its reactors. Such a policy was also adopted by other European countries and by Japan [2]. Another kinds of mixed fuels have been investigating e.g., oxides of thorium/uranium, thorium/plutonium, thorium/transuranic, and transuranic/uranium [1,3-6]. Recently, researchers have been turning their attention to Th fuel cycle in PWRs aiming at reducing the generation of minor actinides, at improving the nuclear power sustainability, and at better fuel utilization and breeding [7-9]. Studies have also discussed the possible role of Th utilization in power reactors and the associated fuel cycles [10].

After reactor discharge, SF must remain under wet storage into SFP until the temperature and the radioactivity emission drop off to safety values for transportation to the final repository. The SFP temperature is controlled by an ECS beneath pre-determined values established according to each country regulation [11], which, typically, should remain between 298 K and 310 K. The Brazil's SFP was designed to store  $UO_2$ -SF discharged from PWRs of the nuclear power plants of ANGRA I and II. The knowledge of the temperature temporal behaviour in an hypothetical scenario of breakdown of the ECS is a requirement for SFP's licensing. Such behaviour is already well-known for the standard  $UO_2$ . However, further analysis including criticality and thermal studies must be conducted for SF originated from thorium-based fuels and reprocessed fuels in view of their possible future utilization in national PWRs.

Concomitant to studies of criticality safety analysis, this research group have been employing efforts to develop thermal simulation studies considering a future scenario of mixed loading pattern of SF into the SFP.

The present work presents thermal studies in the absence of an ECS of the SFP. The modelled SFP follows the loading patterns of assemblies containing mixed SF, which is composed by either  $(U-Th)O_2$  plus  $UO_2$  or  $(TRU-Th)O_2$  plus  $UO_2$  or MOX plus  $UO_2$ .  $T_b$  from such scenarios are also compared with the standard loading of  $UO_2$ -SF. The studies were implemented in the Ansys CFX and OpenFOAM© codes.

## 1.1 THE SFP OF ANGRA II: PREVIOUS SIMULATIONS OF CRITICALITY SAFETY ANALYSIS

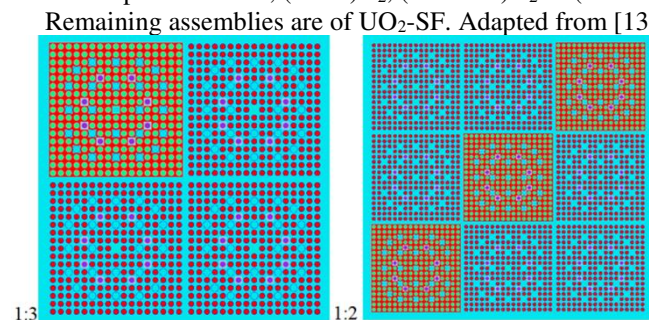
The main characteristics of the SFP are detailed in the Final Safety Analysis Report - FSAR [12]. Its dimensions are 15.914 m x 5.668 m, and 11.6568 m in depth. The fuels assemblies are arranged into the pool in storage racks, obeying the subcriticality regime.

This research group have performed simulations of criticality safety analysis for three different loading patterns designed for assemblies while into the pool [13]. Firstly, a loading pattern with only  $UO_2$  SF was studied. Another analysis considered the SFP fully filled with assemblies of SF, being a quarter of MOX,  $(Th-U)O_2$ ,  $(TRU-Th)O_2$  or  $(TRU-U)O_2$ , and three quarters of standard  $UO_2$ -SF, i.e., a proportion 1:3. Lastly, a loading pattern with the proportion 1:2 was studied, being one assembly of MOX,  $(Th-U)O_2$ ,  $(TRU-Th)O_2$  or  $(TRU-U)O_2$  together with two standard  $UO_2$ -SF assemblies. Figure 1 shows the smallest part of these patterns, called throughout the text as Unit of Repetition (UR), which are replicated until the SFP is fully filled.

The maximum numbers of assemblies into the pool were obtained using a 0.695 cm pitch distance, and maintaining the criticality under the upper multiplication factor limit of 0.95, according to the FSAR [12, 13].

The number of assemblies was 1252 when SFP was entirely filled with only  $UO_2$ -SF. The total of assemblies in the simulated cases were 313 of MOX,  $(Th-U)O_2$ ,  $(TRU-Th)O_2$  or  $(TRU-U)O_2$ , and 939 assemblies of  $UO_2$ -SF for the loading pattern with proportion 1:3. These numbers were 418 of MOX,  $(Th-U)O_2$ ,  $(TRU-Th)O_2$  or  $(TRU-U)O_2$  and 834 assemblies of  $UO_2$ -SF in the pattern with proportion 1:2 [13].

Figure 1. Examples of a unit of repetition of two mixed loading patterns into the pool. The green points arranged in a square lattice represent MOX,  $(Th-U)O_2$ ,  $(TRU-Th)O_2$  or  $(TRU-U)O_2$  assemblies of SF.



## 2 DESCRIPTION OF THE MODEL

This section details the SF properties that are heat sources into the pool. It also describes the geometry of the model, thermophysical properties, boundary and initial conditions, and the meshing of the geometry.

### 2.1 SPENT FUELS PROPERTIES

The main characteristics of SFs include the final amount of fissile material, the burnup and the operation time of reactor were obtained from [13], and are listed in following:

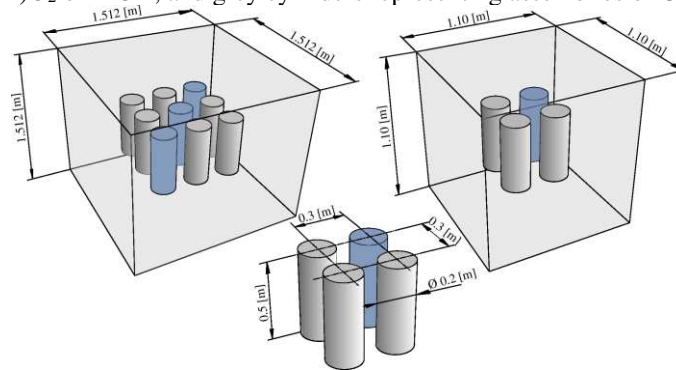
- $\text{UO}_2$ : enriched to 4.3 w/o  $^{235}\text{U}/\text{U}$ ; burnup of 48 GWd/tHM during 3.61 years and 1.634% of final amount of fissile material.
- $(\text{TRU-Th})\text{O}_2$ : fuel composed of 10% of Th and 90% of reprocessed fuel by UREX+, with 9.53% of fissile material; burnup of 48 GWd/tHM during 3.61 years and 6.657% of final amount of fissile material.
- MOX: enriched to 0.25 w/o  $^{235}\text{U}/\text{U}$ ; burn-up of 48 GWd/tHM during 3.61 years and 3.375% of final amount of fissile material.
- $(\text{U-Th})\text{O}_2$ : Enriched to 4.869 w/o  $^{235}\text{U}/\text{U}$ ; burn-up of 48 GWd/tHM during 3.61 years and of 2.084% final amount of fissile material.

### 2.2 GEOMETRY

In this work, the simulated SFP is a representation of the real Angra II pool from Brazil. Each assembly of SF is modelled as a solid cylinder, and only a single UR is represented. To determine the volume of water in the model, the proportion SF/water in the real pool fully filled with assemblies was adopted.

According to the previous studies of criticality safety analysis [13], the maximum volumes of SF into the pool in a loading pattern 1:2 are 20.74 m<sup>3</sup> of reprocessed fuel and 42 m<sup>3</sup> of  $\text{UO}_2$ , and the volume of water is approximately 1,235 m<sup>3</sup>. Therefore, the proportion SF/water is around 0.0508, which is the same in the mixed loading 1:2. Figure 3 shows the modelled SFP that contains a single UR with loading patterns 1:2 and 1:3.

Figure 3. The modelled SFP containing blue cylinders that represent assemblies of (TRU-Th) $O_2$  or (U-Th) $O_2$  or MOX, and grey cylinders representing assemblies of  $UO_2$



### 2.3 SIMULATED CASES

The following studies were addressed considering the modelled SFP loaded according to the pattern 1:2:

- Case I: three cylinders of (TRU-Th) $O_2$  and six of  $UO_2$
- Case II: three cylinders of (U-Th) $O_2$  and six of  $UO_2$
- Case III: three cylinders of MOX and six of  $UO_2$
- Case IV: nine cylinders of  $UO_2$

For the SFP filled according to the pattern 1:3:

- Case V: one cylinder of (TRU-Th) $O_2$  and three of  $UO_2$
- Case VI: one cylinder of (U-Th) $O_2$  and three of  $UO_2$
- Case VII: one cylinder of MOX and three of  $UO_2$
- Case VIII: four cylinders of  $UO_2$

### 2.4 HEAT SOURCES

The heat sources were derived from the decay heat profiles of the SF, at time  $t=0$  year after reactor discharge [13]. To convert from [W/tHM] to [W/m<sup>3</sup>], the values were multiplied by the SF densities. Table 1 shows the heat sources values and their densities.

Table 1. The heat sources values

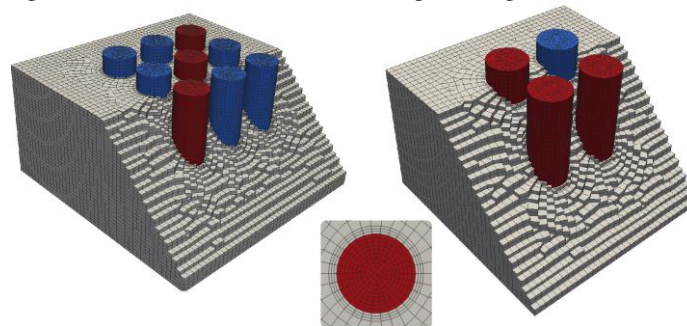
SF type	Density (kg/m <sup>3</sup> )	*Heat source-1 x10 <sup>5</sup> (W/m <sup>3</sup> )	**Heat sources-2 x10 <sup>5</sup> (W/m <sup>3</sup> )
<sup>a</sup> $UO_2$	10830	3.24537	3.24537
<sup>b</sup> $UO_2$		2.08821	2.37162
(TRU-Th) $O_2$	11400	6.86987	6.07654
(U-Th) $O_2$	9510	3.67415	3.49903
MOX	10873	3.10441	3.15659

(\*) and (\*\*) are values for the patterns 1:2 and 1:3, respectively  
(a) Only  $UO_2$ ; (b)  $UO_2$  together with SF from reprocessed fuels

## 2.5 MESHING DATA

The meshes were performed with Ansys CFX meshing tools, and with OpenFOAM© tools. The domains were meshed in different element sizes, depending on their dimensions. Figure 4 shows the mesh of the geometry for the arrangement of nine cylinders (pattern 1:3). The same mesh was used for the arrangement of four cylinders (pattern 1:2).

Figure 4. An illustration of the meshing. The figure is not to scale



Studies of spatial grid convergence were carried out following the Roche's method that is based on the Richardson's extrapolation (ER) [14, 15], and it was applied to the case VIII. The mesh considered appropriated for this case was also used in all other cases. The method requires two or more successively finer grids with a constant grid refinement ratio,  $r$ . It was adopted  $r = 2$ , such that  $N_1 = r N_2 = r^2 N_3$ , with  $N$  being the number of volumetric elements of the domain. Remembering that as greater is  $N$  as finer is the grid, and the grid spacing approaches to zero. Table 2 summarizes the data. The column named as "Normalized grid" corresponds to the mesh normalized by the number of elements of the finer grid to which was attributed the index "1".

Table 2. Data of spatial grid convergence

Normalize dgrid	Nwater	Nfuels	T <sub>b</sub> (h)
1	86720	24960	4.845
2	43360	12480	4.857
4	21680	5852	4.902

Nwater: number of elements of the pool. Nfuels: total number of elements of the cylinders.

The ER may be used to estimate the value of a quantity of interest,  $f$ , at grid spacing  $h = 0$ . In our studies,  $f = T_b$ . For  $r = 2$ , ER may be written as:

$$f_{h=0} \cong \frac{4}{3} \left[ f_1 - \frac{1}{4} f_2 \right] \quad (1)$$

The grid convergence index (GCI) was applied to verify the solution convergence. It is a measure of the percentage that computed values are away from the value of the asymptotic numerical value. It also indicates an error band on how far the solution is from the asymptotic value, and indicates how much the solution would change with a further refinement of the grid. A small value of GCI indicates that the computation is within the asymptotic range. GCI is computed considering values from sequential grids as follows,

$$GCI_{i,i+1} = 1.25 \frac{\left[ \frac{f_i - f_{i+1}}{f_i} \right]}{r^p - 1} \quad (2)$$

where 1.25 is a factor of safety for comparisons over three or more grids, and  $p$  is the solution's order of convergence computed for three sequential grids with the expression:

$$p = \ln \left[ \frac{f_3 - f_2}{f_2 - f_1} \right] / \ln(r) \quad (3)$$

The quantity asymptotic value is assumed to have been reached when,

$$\frac{GCI_{23}}{r^p GCI_{12}} \cong 1 \quad (4)$$

Table 3 summarizes the preliminary grid convergence analysis.

Table 3. Main values of the grid convergence analysis

Quantities	Value
GCI <sub>12</sub>	(*)0.113
GCI <sub>23</sub>	(*)0.421
$p$	1.91

(\*) is in %.  $p$  is the order of convergence



From table 3, the eq. (4) is approximately 1.00248, i.e., the solutions from grids 1, 2 and 3 are within the asymptotic range of convergence. Figure 5 shows the behaviour of  $T_b$  versus the normalized grid (Table 2).

In light of these preliminary studies, the simulated cases V to VIII belonging to the loading pattern 1:3 were meshed according to the grid labelled as “grid 1” (Table 3). For cases I to IV, the parameters were maintained, including the element sizes. The number of elements was 5852 elements in each cylinder of SF, and 175641 elements for the pool. The pool element size was  $3.7 \times 10^{-2}$  m. Each cylinder was meshed by means of the number of division tool on its lids, totalling 42 divisions. The main quality parameters of the mesh are listed in Table 4.

Table 4. Main quality parameters of the adopted mesh

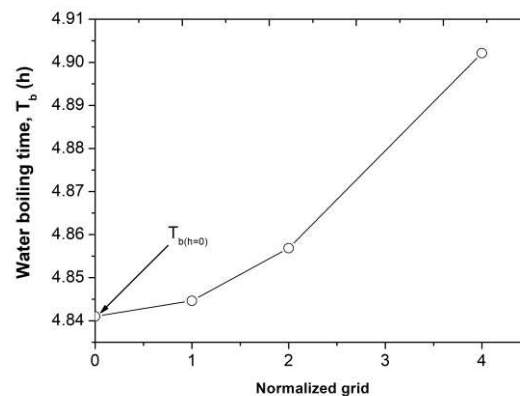
Domain	Maximum aspect of ratio	Maximum no-ortogonality	Average no-ortogonality	Maximum skewness
Cylinders of SF	5.41	20.76	3.54	0.532
Water	5.43	24.62	3.36	

## 2.6 THERMOPHYSICAL PROPERTIES OF MATERIALS

The water properties are from [16], at 298 K. The  $UO_2$  properties, at 673 K, are from [17]. The molar mass of MOX,  $(U-Th)O_2$ ,  $(TRU-Th)O_2$  and  $(U-Th)O_2$  were estimated from their chemical compositions from [13], at 298 K.

The remaining MOX properties are arithmetic means of values between 600 K and 700 K from [18]. The density, specific heat and thermal conductivity of  $(U-Th)O_2$ , at 673 K, are from [19], while its thermal expansivity is from [20] at this temperature.

Figure 5.  $T_b$  versus normalized grid. Plot shows the prediction of  $T_b$  at a continuous grid ( $h=0$ ) according to the ER extrapolation (Eq. 1)



The (TRU-Th)O<sub>2</sub> properties were estimated considering the most significant dioxides present in its composition, which are ThO<sub>2</sub>, PuO<sub>2</sub> and UO<sub>2</sub> [13]. The density, specific heat, conductivity, and thermal expansivity are represented by  $Q$ , and were estimated by the following expression:

$$Q_{(TRU-Th)O_2} = \frac{xQ_{(ThO_2)} + yQ_{(PuO_2)} + zQ_{(UO_2)}}{x + y + z} \quad (5)$$

where  $x$ ,  $y$  and  $k$  are the fractions of ThO<sub>2</sub>, PuO<sub>2</sub> and UO<sub>2</sub>, respectively. These fractions were obtained from [13], whose values are 0.74, 0.093, 0.013, respectively. The dioxides properties were derived from [17, 19], and are arithmetic means in the temperature range from 600 K to 700 K. The properties values are summarized in table 5.

## 2.7 BOUNDARY AND INITIAL CONDITIONS

The k-epsilon turbulence and buoyancy models were adopted in the pool domain, whose walls, including the top, were set as adiabatic. The pressure in water was set as 1 atm. The initial temperatures were: 298 K for water and 673 K for cylinders of SF. The latter value is the temperature of an assembly of SF at the nuclear reactor shutdown.

$T_b$  is the mean temperature of the water, being averaged over the whole water volume. Figure 6 shows the main boundary and initial conditions of the model.

Figure 6. The boundary and initial conditions of the model

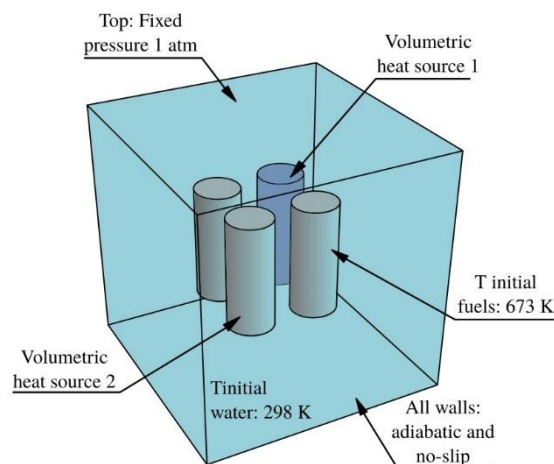


Table 5. Thermophysical properties of materials

SF type	Density [kg/m <sup>3</sup> ]	Molar mass [kg/kmol]	Specific heat [J/(kg.K)]
*Water	997.1	18.02	4183
UO <sub>2</sub>	10830	270	297
(TRU-Th)O <sub>2</sub>	11400	265	276.5
(U-Th)O <sub>2</sub>	9510	202.83	362.4
MOX	10873	207	297.9
SF type	$\lambda$ [W/(m.K)]	Thermal expansivity x10 <sup>-6</sup> [K <sup>-1</sup> ]	
Water	0.5948	259.4	
UO <sub>2</sub>	4.74	10	
(TRU-Th)O <sub>2</sub>	3.065	8.604	
(U-Th)O <sub>2</sub>	5.2	8.0	
MOX	2.48	9.9	

### 3 RESULTS AND DISCUSSION

The results were compared among them by using both ANSYS CFX and OpenFOAM© codes.

#### 3.1 T<sub>B</sub> FROM SIMULATIONS WITH LOADING PATTERN 1:2: CASES I, II, III, AND IV

Cases I, II, III represent mixed storages, where the three cylinders of SF of a single diagonal (see Figure 1, right) are either (TRU-Th)O<sub>2</sub> or (U-Th)O<sub>2</sub>, or MOX, and the remaining are UO<sub>2</sub>. Case IV is the standard storage with only UO<sub>2</sub>.

Figure 7 shows the temporal behaviour of the water temperature in the absence of an ECS for the pool. T<sub>b</sub> from each case is listed on Table 6.  $\Delta T_b$  is the difference between T<sub>b</sub> obtained from each case and the standard case of UO<sub>2</sub> (case IV).

#### 3.2 T<sub>B</sub> FROM SIMULATIONS WITH LOADING PATTERN 1:3: CASES V, VI, VII, AND VIII

Cases from V, VI and VII represent mixed storages, where one of the four cylinders of SF is (TRU-Th)O<sub>2</sub> or (U-Th)O<sub>2</sub>, or MOX, and the remaining are UO<sub>2</sub> (see Figure 1, left). Case VIII is the standard storage with only UO<sub>2</sub>.

Figure 8 shows the temporal behaviour of the water temperature. T<sub>b</sub> from each case is listed on Table 7.

As expected,  $T_b$  values from loading pattern 1:2 are lower than those ones when SFP is loaded following the pattern 1:3 since there is more heat being transferred to the water in the arrangement containing more assemblies of reprocessed fuels.

Even though the heat source value of the (U-Th) $O_2$  SF is higher compared to that of  $UO_2$ , (Table 1),  $T_b$  from the cases of (U-Th) $O_2$  together with  $UO_2$  is greater than  $T_b$  from the cases with only  $UO_2$  in both loading patterns. This observation can be explained by the higher specific heat value of the (U-Th) $O_2$  in comparison to that of  $UO_2$  (Table 5). The same observation can be verified for the case VII (MOX together with  $UO_2$ ). In light of the heat source value of MOX (Table 1),  $T_b$  would be lower than that from the case VIII (only  $UO_2$ ). However, as can be seen in table 5, thermal conductivity,  $\lambda$ , of MOX is lower than that of  $UO_2$ . Although its specific heat is higher, in this situation, it seems that  $\lambda$  has the major influence in the heat propagation.

As can be seen from Figures 7 and 8, the smallest differences between ANSYS and OpenFOAM© results are verified for simulations with only  $UO_2$ . In simulations with two heat sources, the divergence between the codes enhanced with the time. The present studies are unable to explain such differences since all the simulation parameters are essentially the same in both codes. Further studies will be necessary to clarify it.

In both SFP's loading patterns, the difference ( $\Delta T_b$ ) between  $T_b$  from each simulated case and the standard case of  $UO_2$  has the higher value for MOX (tables 6 and 7), whilst the mixed loading of (TRU-Th) $O_2$  together with  $UO_2$  has the lowest  $\Delta T_b$ . It means that, in case of breaking down of the ECS, SFP would reach the saturation temperature more quickly when it is loaded with the combination of (TRU-Th) $O_2$  and  $UO_2$ , and it would take more time to reach this temperature when loaded with the combination of MOX and  $UO_2$ , independent of the loading pattern.

Table 6.  $T_b$  from the loading pattern 1:2 – Cases from I to IV

Cases	$T_b$ (h)		$\Delta T_b$ (min)	
	Ansys	Open FOAM	Ansys	Open FOAM©
I	4.05	3.48	-28.8	-51.6
II	5.27	4.67	44.4	19.8
III	5.89	5.21	81.6	52.2
IV	4.53	4.34	-----	-----

Figure 8.  $T_b$  versus normalized grid. Plot shows the prediction of  $T_b$  at a continuous grid ( $h=0$ ) according to the ER extrapolation (Eq. 1)

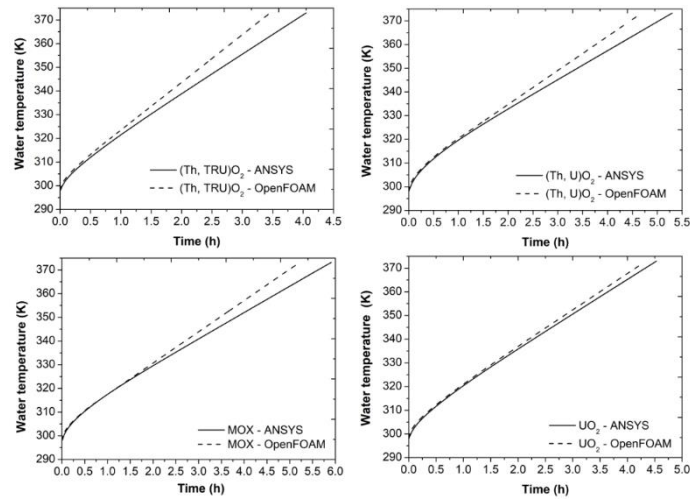
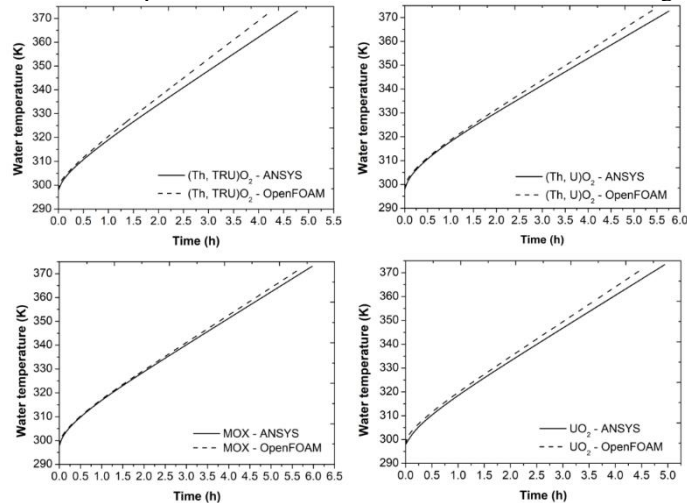


Table 7  $T_b$  from the loading pattern 1:3– Cases from VI to VIII.

Cases	$T_b$ (h)		$\Delta T_b$ (min)	
	Ansys	Open FOAM	Ansys	Open FOAM©
V	4.78	4.25	-1.8	21.6
VI	5.79	5.40	58.8	47.4
VII	5.97	5.77	69.6	69.6
VIII	4.81	4.61	-----	-----

Figure 7. Water temperature behaviour when SFP is loaded according to the pattern 1:3



#### 4 CONCLUSION

This work presented studies of the time in which a simulated spent fuel pool takes to reach the water boiling time in the absence of an external cooling system. Three different loading patterns of spent fuel assemblies were studied. The modelled pool is a

simplification of that from Angra II, Brazil, and consisted on a smallest unit of repetition of its loading patterns.

It was verified that when the simulated spent fuel pool was loaded with (TRU-Th) $O_2$  together with  $UO_2$ , it reaches 373 K more quickly than any other kind of loading. In contrast, it takes more time to reach this temperature when the loading is with MOX together with  $UO_2$ . The differences found in the water boiling times resulted from a balance between the heat source intensities, specific heat and thermal conductivity of the spent fuels.

The simulations were carried out with two codes – ANSYS and OpenFOAM©. Both yielded similar results, although major differences were observed in results from simulations with two different heat sources. Additional studies might be required to investigate these differences.

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